

(An ISO 3297: 2007 Certified Organization) Vol. 4, Issue 11, November 2015

Optimization of Grain Layer Thickness in the Design of Solar Grain Dryer through Simulation

Mr. Booker Osodo¹, Prof. Daudi Nyaanga², Dr. Jeremiah Kiplagat³, Dr. George Owino⁴

ecturer, Department of Industrial and Energy Engineering, Egerton University, B. Osodo, Nakuru, Kenya¹

Associate Professor, Department of Agricultural Engineering, Egerton University, D. Nyaanga, Nakuru, Kenya²

Principal, Kenya Power and Lighting Company Training School, J. Kiplagat, Nakuru, Kenya³ Lecturer, Department of Industrial and Energy Engineering, Egerton University, G. Owino, Nakuru, Kenya⁴

ABSTRACT: Forced convection solar dryers, utilizing solar driven fans, may be used to improve ventilation, and to achieve an optimum drying air velocity in grain dryers. However, without use of the appropriate grain layer thickness, the heated air may not be able to successfully penetrate the grain to facilitate drying. Also, too many grain layers placed in the drying cabinet may prevent air from flowing up the entire drying cabinet. The appropriate grain layer thickness and maximum number of drying trays are therefore factors that are crucial in sizing a solar drying cabinet. However, their determination, without use of simulation, would require troublesome development stages, involving trial and error and continued testing, a process which would be expensive and time consuming. This study applied simulation using Comsol Multiphysics Software for their determination, hence enabling the sizing of a dryer cabinet to facilitate sufficient and effective aeration of the grain for optimization of the drying process. It was found that the maximum grain layer thickness that can allow penetration by air is 100 mm. It was also found that the maximum number of grain layers that should be dried for effective aeration was 4.

KEYWORDS: Optimisation, Solar Drying, Grain Layer Thickness, Comsol Multiphysics Software, Deep bed drying.

I. INTRODUCTION

In developing countries, post-harvest food losses are estimated to be of the order of 40%, but can rise to be as high as 80% under very adverse conditions. A significant percentage of these losses is related to improper and, or untimely drying of foodstuffs, since one reason for loss of grain after harvesting is spoilage resulting from high moisture content, according to the authors in [4] and [5]. In [3] and [6], it is stated that incidences of post-harvest food loss in Kenya have been estimated at 30%, and can rise to be as high as 100% with the advent of afflotoxin. Drying of maize to below 13.5% moisture content increases storage life and maintains quality by decreasing growth of fungi and insect infestation during storage. It also prevents germination.

Solar drying is preferred to drying using other sources of energy since it is abundant, inexhaustible and non-polluting. Also, drying using solar energy leads to conservation of conventional energy sources [2].Open sun drying (OSD) has several disadvantages, such as loss to rodents, birds and other pests; cracking and discoloration; over drying, insufficient drying, contamination by foreign materials [12].Other modes of grain drying are direct solar drying (DSD), and indirect solar drying (ISD). DSD utilizes the green house effect to dry crop placed in an enclosure covered with a transparent cover, the crop being directly exposed to solar radiation. Although the grain is protected from adverse weather conditions, it is still prone to cracking and discoloration inside the glass cover reduces the transitivity of the glass. Some of the limitations of DSDs are addressed by ISDs, in which heated air from a separate solar collector is passed through the crop, placed in a separate chamber [12].



(An ISO 3297: 2007 Certified Organization)

Vol. 4, Issue 11, November 2015

An optimum air flow rate is essential for achieving a satisfactory dryer performance. Slower air flow rate may increase drying air temperature while higher air flow rate may decrease moisture removed, according to the authors in [1] and [9].In [11], it is stated that factors affecting drying rate include air temperature, air velocity and grain layer thickness, among others. Thus, without knowledge of the optimum air velocity and grain layer thickness for optimum drying rate and for ensuring no damage to the grain, optimum performance of a solar grain dryer will not be attained, as stated in [13]. In [8], it is shown that typical air flow rates range from 0.25-0.51 m³/ s m² of perforated screen area, these flow rates creating relatively low static pressures of 0.249-1.25 kPa in cross flow and mixed-flow dryers.

A grain layer thickness that allows air to flow through the grain at an optimum rate is therefore essential if the drying process is to be effective. Determination of this thickness is crucial in the proper design of a grain dryer. Knowledge of the grain layer thickness, and hence also height of void space, enables determination of drying cabinet dimensions, once the number of layers penetrable by the air is determined. However, determination of these parameters, without use of simulation, would require troublesome development stages, involving trial and error and continued testing, a process which would be expensive and time consuming. This study applied simulation using ComsolMultiphysics software for their determination. This enabled the sizing of a dryer cabinet to facilitate sufficient and effective aeration of the grain for optimization of the drying process.

II. PERFORMANCE OPTIMIZATION

Simulation was carried out of hot air flowing through a single grain layer of 50mm thickness, at an air velocity of 1m/s. A parametric sweep was then carried out in order to simulate air flow through different grain layer thicknesses ranging between 50 mm - 300 mm. This was in order to determine the optimal grain layer thickness that would allow the fan to overcome the static pressure resulting from airflow. Once the optimal grain layer thickness was determined, simulation to determine the pressure drop up a single layer of grain was done. The number of layers was then increased gradually to study the pressure profiles for increasing number of layers, in order to determine the number of drying trays that would be used in the dryer to allow air penetration up the drying chamber. The assumption made was that the grain behaved like a packed bed. According to [7] and [10], fluid flow through a packed bed may be described using the Ergun equation (eq. 1). According to this equation, pressure drop along a packed bed given some fluid velocity depends on packing size, length of bed, fluid viscosity and fluid density.

$$\frac{\nabla p}{L_p} = \frac{150\mu (1-\varepsilon)^2 u_0}{\varepsilon^3 d_p^2} + \frac{175 (1-\varepsilon)\rho\mu^2}{\varepsilon^3 d_p}$$
(1)

Where

 $\nabla P = \text{Pressure drop} \qquad \mu = \text{Absolute viscosity of fluid} \\ L_p = \text{Length of bed} \qquad d_p = \text{Effective diameter of particles assumed to be equivalent to spheres} \\ \varepsilon = \text{Fractional void volume of bed} \qquad \rho = \text{Density of fluid} \\ \mu_0 = \text{Superficial fluid velocity}$

III. EXPERIMENTAL SET-UP AND RESULTS

Airflow up single layers of various thicknesses ranging between 50mm-300mm, at 50 mm intervals, were simulated. In each case, the inlet air velocity of 1m/s was used. In the case of grain layer thickness of 50mm, as shown in fig.1, a linear increase in air velocity up the grain layer until an approximate height of 2.3 mm was observed, after which the air velocity fell. The air velocity was also much lower than the inlet velocity (between 0.034 - 0.07 m/s for inlet velocity 0f 1 m/s). This showed that the static resistance to air flow was much higher than the fan could overcome, suggesting that this would not be an appropriate grain layer thickness.



(An ISO 3297: 2007 Certified Organization)



For a grain layer thickness of 100 mm shown in fig.2, air velocity increased gradually up the entire grain layer, levelling off at the top implying that this would be an appropriate grain layer thickness for the dryer, and that the suction fan would be able to overcome the static pressure.

For grain layer thickness of 150 mm in fig.3, the graph showed that the air completely failed to flow up the grain layer. This was probably because the suction fan was totally unable to overcome the static pressure (resistance to airflow). Thus, this would not be an appropriate grain layer thickness to use for the dryer. Fig.4 shows that for grain layer thickness of 200mm, air velocity increased up to a grain layer height of 40 mm, before falling sharply. Air velocity was again observed to be increasing sharply at the upper section of the grain layer. However, because the expectation was for the air velocity to rise steadily up the grain layer, it was concluded that this was also not an appropriate grain layer thickness to use.



For a 250mm grain layer thickness as in fig.5, air velocity increased up the grain layer, but only up to a height of 30mm before decreasing, showing again that this was not an appropriate grain layer thickness to use.





In the case of 300mm grain layer thickness in fig.6, once again air velocity increased up the grain layer, but the increase was not sustained. The velocity dropped way before the top of the grain layer, at a height of about 200 mm. This showed that this was not an appropriate grain layer thickness to use.

Fig. 7 is a graph showing pressure drop for a single 100 mm layer. It indicates that there is a linear drop in pressure from the lower section of a grain layer upwards, the total pressure drop for a 100 mm single layer being 1.2×10^4 Pa. There is a similar trend as the number of grain layers is increased until the number of layers is 4, as shown in fig. 8.



Beyond 4 grain layers, the linear trend in pressure decline ceases. For example, it is evident from figs. 9 and 10 that for 5 and 8 grain layers respectively, there are sections where there is little or no change in pressure, suggesting that there is little or no air flow.





This trend intensifies to the extent that for 16 grain layers and beyond, there is no pressure drop at all showing no air flow through the grain layers. This, for example, is shown in fig. 11 for 16 layers.



IV. CONCLUSION

It was concluded that the grain dryer should be loaded with a maximum of 4 trays, each with grain layer thickness of 100 mm. These conditions, if applied, would allow sufficient aeration of the grain and hence facilitate effective drying.

V. ACKNOWLEDGEMENT

My gratitude goes to Kenyatta University that has given me the opportunity to carry out this project in partial fulfilment of the PhD program.



(An ISO 3297: 2007 Certified Organization)

Vol. 4, Issue 11, November 2015

REFERENCES

- [1] Afriyie, J.K., Nazha, M.A.A., Rajakaruna, H. & Forson, F.K. (2009). Simulation and Optimisation of the Ventilation in a Chimney Dependent Solar Crop Dryer. Solar Energy 4: 1560-1573
- [2] Akinona, O.A., Akinyemi, A.A. & Bolaji, B.O. (2006).Evaluation of Traditional and Solar Fish Drying Systems towards Enhancing Fish Storage and Preservation in Nigeria. Fish International: Pakistan 1(3):44-49
- [3] Barawal, P. &Tiwari, G.N. (2008).Grape Drying by Using Photovoltaic Thermal (PV/T) Green House Dryer: An Experimental Study of Solar Energy. Solar Energy. 62(12): 1131-1144.
- [4] Bolaji, B.O. & Alalusi, A.P. (2008). Performance Evaluation of a Mixed Mode Solar Dryer. AU.J.T 11(4):225-231.
- [5] Hodges, R.(2009). Supplying Cereal Grain Postharvest Losses Information: the Examples of ALPHIS (African Postharvest Loss Information System. Natural Resources Institute, UK. Retrieved from http://www.rsis.edu.sg/nts/doc/session%20420Hodgespdf on 13th May 2013
- [6] Irungu, J. (2010) Post Harvest Challenges to Food Security in Kenya. A paper presented at KCB Leadership Center, Karen, Nairobi
- [7] Jia, Y., Li, Y. & Hlavka, D. (2009). Flow through Packed Beds. http://www.me .rochester.edu/courses/ME241/11-sand.pdf
- [8] Maier,D.E. & Bakker-Arkema, F.W.(2002).Grain Drying Systems.Paper presented at Facility Design Conference of Grain Elevator and Processing Society held on July 28-31 in St Charles, Illinois,USA
- [9] Murthy, M.V.R. (2009). A review of new Technologies, Models and Experimental of Solar Dryers. Renewable and Sustainable Energy Reviews 835-844
- [10] Sachdeva, S., Pareek, S., Mahadevan, B.& Deshapande, A.(2012). Modeling and Simulation of Single Phase Fluid Flow and Heat Transfer in Packed Bed. Proceedings of 2012 COMSOL Conference, Bangalore
- [11] Sevik, S. (2013). Design, Experimental Investigation and Analysis of a Solar Dryer System. Energy Conversion and Management 68:227-234
- [12] Tiwari, G.N. (2002). Solar Energy: Fundamentals, Design, Modeling and Applications. Parybourne: Alpha Science International Limited
- [13] Wilcke, W.F. & Morey, R.V. (2015). Selecting fans and determining airflow for crop drying, cooling, and *storage*. Retrieved September 2015