

EFFICIENCY WITH DIFFERENT GCV OF COAL AND EFFICIENCY IMPROVEMENT OPPORTUNITY IN BOILER

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Abstract: Boiler is a most useful device for any developing industries to process & production. It is necessary to optimized good boiler efficiency. Boiler efficiency can be measured by two method, direct method and indirect method. Both methods give a different result. Direct method did not include any losses for calculating boiler efficiency, while indirect method includes all the heat losses from a system to find boiler efficiency. This paper gives simulating with the various value of the fuel. GCV of fuel indicate the heating value of fuel. As the heating value is high, efficiency is also increased with increased with the higher GCV coal. Compare with the different GCV of coal to find out the proper fuel selection of fuel. There are different parameters regarding to the boiler system which helps to improved boiler efficiency.

Keywords: boiler efficiency, GCV of coal, increase in efficiency, comparison, efficiency improvement opportunity

Nomenclatures

Q_o = Heat output

Q_i = Heat input

Q = Quantity of steam generated per hour (kg/hr)

q = quantity of fuel per hour (kg/hr)

hg = steam enthalpy (kcal/kg)

hf = feed water enthalpy (kcal/kg)

GCV of fuel = gross calorific value of fuel (kcal/kg)

C_p = specific heat of flue gas (0.23 Kcal/kg^oC)

T_f = temperature of flue gas (^oC)

T_a = ambient temperature (^oC)

T_s = surface temperature (^oC)

m = mass of dry flue gas (kg/kg of fuel)

H_2 = percentage of H_2 in fuel = kg of H_2 in 1kg of fuel

C_p = specific heat of superheated steam (0.45 Kcal/kg^oC)

584 = latent heat of water in Kcal/kg

M = % of moisture present in fuel = kg of moisture in 1kg of fuel

C_p = specific heat of super-heated steam (0.45 Kcal/kg^oC)

AAR = actual air required (kg/kg of fuel)

M_{bw} = mass of blow down water (Kg/hr)

H_{bw} = enthalpy of blow down water at drum pressure (Kcal/kg)

H_{fw} = enthalpy of feed water (Kcal/kg)

M_a = mass of total ash generated/kg of fuel

SBC = Steffen Boltzmann constant ($5.67 * 10^{-6}$)

ϵ = emissivity factor of surface

A = total surface area (m²)

C = 1.97 for vertical surface

= 2.56 for upward facing horizontal surface

= 1.32 for downward facing surface

= 2.30 for horizontal cylindrical surface

I. INTRODUCTION

Boiler is a steam generating device, which produce steam with burning of fuel. Basically coal is used as fuel in boiler. If the fuel has higher gross calorific value, than it is able to produce more heat per kg of fuel. It is directly proportional

to the efficiency. Efficiency of the boiler should be calculated by two method, direct method and indirect method. It required various parameters for calculating the efficiency. These parameters are chemical analysis result of coal, feed waters analysis, coal feeding rate, steam pressure, steam generation per hour, flue gas analysis, and weather any heat recovery devices are attach or not, if attach, than its data, fuel consumption rate per hour, humidity factor etc. These all are related to each other and required for calculation.

The mathematical model in the Microsoft excel is prepared for the indirect method for finding boiler efficiency, because these method has a lots of calculation which make us a bore if the same calculation is required for the different value of GCV of coal. By using Microsoft excel the repeated calculations are being quite easy and time saving. Just change the various values and at the last you got the result immediately without any handwritten time consuming paperwork.

Here calculation has been done for the 40THP FBC boiler used in the L & T Industries, fuel having GCV of 5800 kcal/kg and 4300 kcal/kg respectively for semi bituminous coal and Indian lignite coal. Both coals have a different chemical composition and properties.

There are lots of possibilities to improve boiler efficiency by taking necessary steps for different parameters which are directly affected to the boiler efficiency. By considering them it gives an opportunity to improve boiler efficiency.

II. METHODS TO CALCULATE THE BOILER EFFICIENCY.

There are two methods to find out boiler efficiency.

1. Direct method
2. Indirect method

1. Direct method:-

Boiler efficiency is calculated with this formula

$$\text{Boiler efficiency} = \frac{\text{Heat output}}{\text{Heat input}}$$

$$\begin{aligned} \text{Boiler efficiency } \eta &= \frac{Q_o}{Q_i} * 100 \\ &= \frac{Q * (h_g - h_f)}{q * \text{GCV of fuel}} * 100 \end{aligned}$$

2. Indirect method

By this method, efficiency could be measured easily by measuring all the losses occurring in the boiler.

The following losses were applicable to all the fuel used, weather it is solid, liquid or gas fired boiler.

- L1 – loss due to dry flue gas
- L2 – loss due to hydrogen in fuel
- L3 – loss due to moisture in fuel
- L4 – loss due to moisture in air
- L5 – loss due to CO formation
- L6 – loss due to un-burnt fuel in fly ash
- L7 – loss due to un-burnt fuel in bottom ash
- L8 – loss due to radiation and convection (surface loss)

$$\begin{aligned} \text{Boiler efficiency } \eta &= 100 - \text{Total losses} \\ &= 100 - (L_1 + L_2 + L_3 + L_4 + L_5 + L_6 + L_7 + L_8) \end{aligned}$$

III. FORMULA FOR COMPUTATING VARIOUS LOSSES

Step 1. Theoretical (stoichiometric) air requirement

$$\text{Theoretical air requirement (TA)} = \frac{11.6C + 34.8 \left(h_2 - \frac{O_2}{8} \right) + 4.35S}{100} \text{ kg/kg of fuel}$$

Step 2. % excess air requirement

$$\% \text{ excess air requirement (EA)} = \frac{O_2\%}{21 - O_2\%} * 100$$

Step 3. Actual air (total air) requirement

Actual air (total air) requirement (AAR) = theoretical air * $(1 + \frac{EA}{100})$ kg of air/kg of fuel

Step 4. Find all heat loss

1. Dry flue gas loss

$$\begin{aligned} \text{\% heat loss due to dry flue gas} &= \frac{m \cdot C_p (T_f - T_a)}{GCV} * 100 \\ &= \text{mass of CO}_2 + \text{mass of SO}_2 + \text{mass of N}_2 + \text{mass of O}_2 \text{ (water vapor mass is neglected)} \\ &= \left(\frac{C}{100} * \frac{44}{12}\right) + \left(\frac{S}{100} * \frac{64}{32}\right) + \left(AAR * \frac{77}{100}\right) + \left[(AAR - T_a) * \frac{23}{100}\right] \end{aligned}$$

2. Heat loss due to evaporation of water formed due to H₂ in fuel

$$= \frac{9 * H_2 * [584 + C_p (T_f - T_a)]}{GCV} * 100$$

3. Heat loss due to evaporation of moisture in fuel

$$= \frac{M * [584 + C_p (T_f - T_a)]}{GCV} * 100$$

4. Heat loss due to moisture in combustion air

$$= \frac{AAR * \text{humidity factor} * C_p (T_f - T_a)}{GCV} * 100$$

C_p = specific heat of super-heated steam (0.45 Kcal/kg°C)

Humidity factor = % of water in dry air

$$= \frac{\text{kg of water in dry air}}{\text{kg of dry air}}$$

5. Heat due to un-burnt in fly ash

$$= \frac{M_a * GCV \text{ of fly ash}}{GCV \text{ of fuel}} * 100$$

6. Heat loss due to un-burnt in bottom ash

$$= \frac{M_a * GCV \text{ of bottom ash}}{GCV \text{ of fuel}} * 100$$

7. Blow down loss

$$\text{\% blow down loss} = \frac{M_{bw} * (h_{bw} - h_{fw})}{GCV \text{ of fuel}} * 100$$

8. Heat loss due to radiation & convection

= 1 to 2% for smaller capacity boiler

= 0.2 to 1.2 for large capacity boiler

% surface heat loss = radiation loss + convection loss

$$\text{\% radiation loss} = \frac{SBE * \epsilon * A * (T_s^4 - T_a^4) * 860}{GCV \text{ of fuel} * 1000}$$

$$\text{\% convection loss} = \frac{C * A * (T_s - T_a)^{1.25} * 860}{GCV \text{ of fuel} * 100}$$

Step 5: find sum of all heat losses

% total losses = sum of all heat losses

$$= 1 + 2 + 3 + 4 + 5 + 6 + 7 + 8$$

Step 6: estimate boiler efficiency

$$\eta_B = 100 - (1 + 2 + 3 + 4 + 5 + 6 + 7 + 8)$$

$$\% \eta_B = 100 - (\% \text{ total losses})$$

I. THE FOLLOWING DATA IS TAKEN FOR FIND OUT BOILER EFFICIENCY OF DIFFERENT GCV OF COAL.

Efficiency measurement is carried out on the 40THP FBC boiler at L&T Industries, Surat. Performance test is carried out with semi bituminous coal and then simulate with Indian lignite coal for achieved difference efficiency.

Fuel Type	Indian lignite coal fired	Semi bituminous coal type
Steam generation rate	40000 kg/hr	40000 kg/hr
Operation hours	7200 hrs/year	7200 hrs /year
Steam pressure	32 kg/cm ²	32 kg/cm ²
Steam temperature	380 °C	380 °C
Coal firing rate	5846 kg/hr	4300 kg/hr
GCV of fuel	4300 kcal/kg	5800 kcal/kg
Total surface area	150 m ²	150 m ²
Surface temperature	210 °c	210 °C
Wind velocity	3.9 m/s	3.9 m/s
Ambient temperature	33 °C	33 °C
Humidity factor	0.021 kg/kg of dry air	0.021 kg/kg of dry air

A. Feed water analysis from laboratory

Feed water temperature	160 °C	160 °C
TDS	200 ppm	200 ppm
pH	7.1	7.1

B. Ultimate analysis of coal from laboratory

C	37%	59%
H ₂	2.9%	3.1%
N ₂	1.1%	1.1%
O ₂	4.5%	10.4%
Ash	36%	12.1%
Moisture	17%	12.9%
Sulphur	1.5%	1.4%

C. Flue gas analysis with flue gas analyzer

Flue gas temperature	600 °C	600 °C
% O ₂ in flue gas	8.12%	8.12%
% CO ₂ in flue gas	11.6%	11.6%
% CO in flue gas	0.42%	0.42%

D. Ash analysis

GCV of bottom ash	700 kcal/kg	700 kcal/kg
GCV of fly ash	150 kcal/kg	150 kcal/kg
Bottom ash to fly ash ratio	45:55	45:55

I. RESULT FROM CALCULATION

Result derived from the above formulas for the fuel Indian lignite coal with GCV of 4300 kcal/kg and semi bituminous coal with GCV of 5800 kcal/kg is shown in table 1 and 2.

Table No 1
Result of Boiler Efficiency Calculation

	Indian Lignite coal	Semi bituminous coal
Theoretical air requirement (kg/kg of coal)	7.5313	7.5313
% Excess air required for complete combustion of coal		
Method 1	63.04%	63.04 %
Method 2	10.25%	63.34 %
Method 3	11.30%	64.85 %
Actual Air Requirement (kg/kg of coal)	8.303	12.302
Mass Of Dry Flue Gas Exhausted From Stack	8.845	13.243
Heat Loss In Dry Flue Gas	8.245%	6.112 %
Heat Loss Due To H ₂ In Fuel	4.814%	5.146 %
Heat Loss Due To Moisture In Fuel	2.625%	1.477 %
Heat Loss Due To Moisture In Air	0.3248%	0.3567%
Heat Loss Due To CO Formation (Incomplete Combustion)	1.727%	2.041%
Heat Loss Due To Un-burnt Fuel In Fly Ash	0.2321%	0.3442 %
Heat Loss Due To Un-burnt Fuel In Bottom Ash	0.8863%	0.6571 %
Heat Loss Due To Radiation And Convection (kcal/m ²)	6078.301	6078.3
Surface Loss	3.626%	3.655 %
Boiler Efficiency	77.51	80.20 %

Table No 2.
Efficiency Find Out by Direct and Indirect Method

Boiler efficiency	Indian lignite coal	Semi bituminous coal
Indirect method	77.51	80.20
Direct method	79.05	79.68

VI. GRAPHICAL ANALYSIS OF RESULT

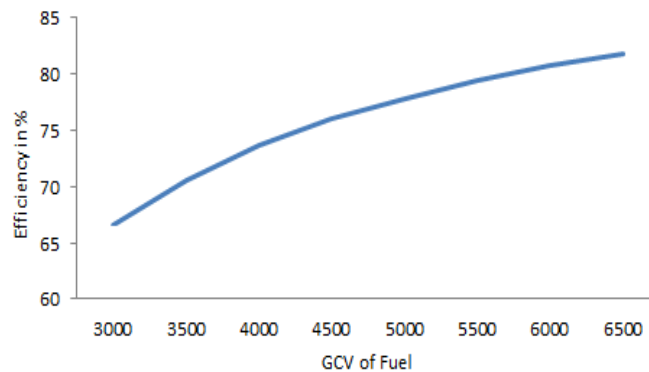


Fig 1 efficiency with GCV of coal

Figure 1 shows the boiler efficiency with the GCV of the coal. As the coal used with higher GCV, efficiency is increased. Lignite coal with 4300 kcal/kg gives a 77.51% in this boiler, while semi bituminous coal with 5800 kcal/kg gives 80.20% efficiency in this boiler. So as the higher grade coal is used, efficiency will be increase.

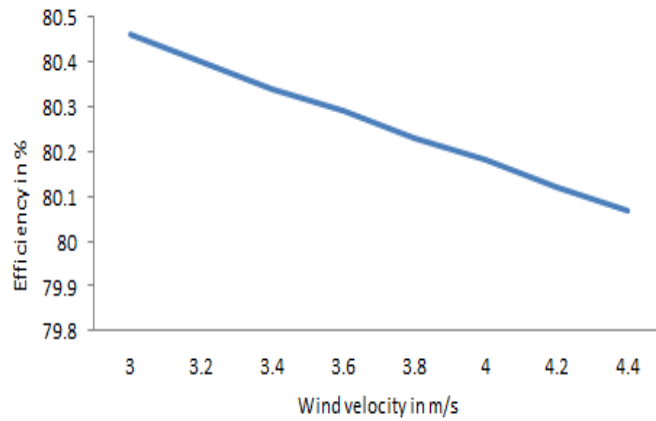


Fig 2 efficiency with wind velocity

Figure 2 shows that while wind velocity is increased that time surface loss is increased so the efficiency is decreased.

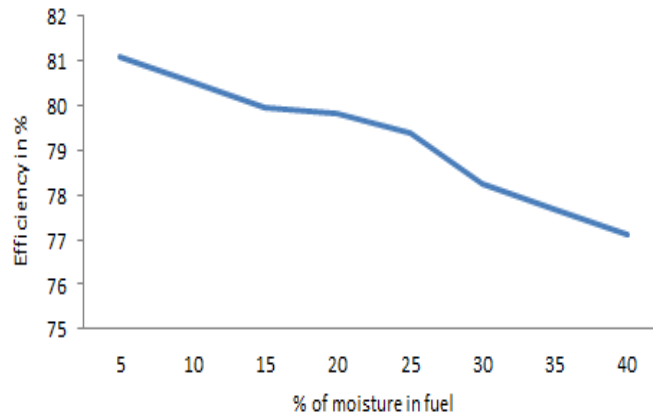


Fig 3 Efficiency with % of moisture in fuel

Figure 3 indicate that if fuel is moister, than it is directly affected the combustion of fuel, so increasing in the moisture content in the fuel means decreasing in efficiency.

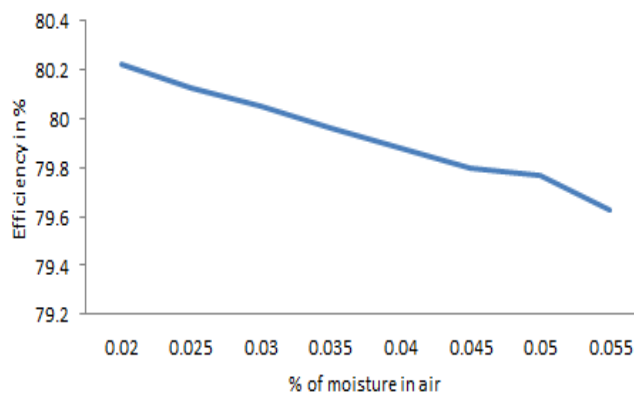


Fig 4 efficiency with % of moisture in air

Figure 4 shows the effect of moist air on the boiler efficiency. It is called seasonal effect.in the monsoon season air is more humid, and in summer and winter the air is dry. Air has less water particles in the summer and winter. So as the moisture content in air is increased the efficiency of the boiler is decreased.

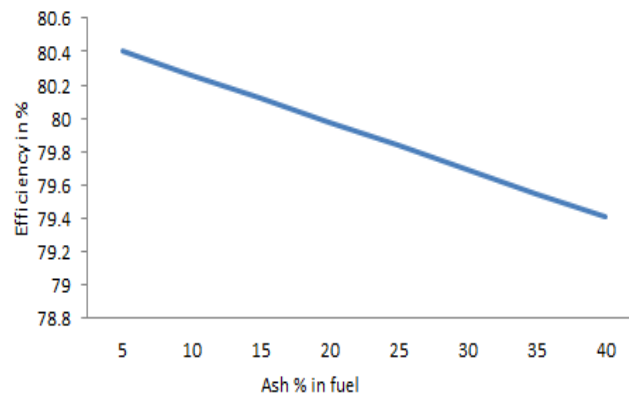


Fig 5 Efficiency with ash % in fuel

Figure 5 show that the coal has a more ash content; it decreased the efficiency of the boiler. Lignite coal has up to 40% ash content and other high grade coal like semi bituminous and bituminous have less ash content than the other coal. So increasing in % of ash in coal is result in a decreasing of efficiency.

VII. EFFICIENCY IMPROVEMENT OPPORTUNITY IN BOILER SYSTEM

These are the parameters which are useful for improvement of the boiler efficiency.

A. Proper water treatment:

Various forms of contaminations arise with water and they must be removed before feeding to the boiler system by proper water treatment. Otherwise they moves with water and concentrate in the boiler, as a result deposition and scales are form which may reduce the heat transfer, reduce the boiler efficiency, increase the operation & management cost and damage the tubes.

I. TDS control

Total dissolves solids comes with feed water into the boiler, water is heated and converted into the steam bur TDS are remaining in the boiler and concentrated, and eventually reach at a level where their solubility in the water in the water is exceeded and they deposit from the solution. Thus they form scale and reduce heat transfer and also overheat the tubes and puncture those tubes. Thus TDS control is essential by manual blow down or automatic blow down system.

II. pH control

pH is the measure of how acidic or basic the feed water. Feed water must be neutral which save the energy. pH is controlled by either removing impurities or adding other chemicals to neutralized the water or by blow down of water.

B. Proper fuel preparation:

Fuel contaminants (dirt, dust, suspended particles, moisture etc.) , they must be removed by proper fuel treatment otherwise, they forms the scales and reduces the heat transfer rate or excessive moisture uses a lot of energy as required to change the phase and this energy carried over with flue gas as loss. A quality feed into the boiler raise the efficiency level of boiler and also reduce the maintenance costs.

C. Fuel selection:

The proper fuel specification can also have a effect on efficiency. In the case of gaseous fuel, the higher the hydrogen content, the more water vapor is formed during combustion, which leads higher heat loss due to evaporation of water form by hydrogen in fuel. To get an accurate efficiency calculation, a fuel specification that represents the job site fuel to be fired must be used.

D. Eliminate incomplete combustion:

The heat produced from incomplete combustion of fuel is less compared to complete or good combustion of fuel. It is ultimately a heat loss.

The main causes of incomplete combustion are:

- Excess fuel supply
- Shortage of combustion air
- Improper firing of fuel
- Improper sizing of fuel (in case of solid fuels)
- Poor atomization of fuel (in case of liquid fuel)
- Poor mixing of fuel and air

A proper selection, operation and good servicing of burner system can reduce the problems of incomplete combustion. In coal firing system, un-burnt coal found in the bottom ash or carried over with flue gas or fly ash. This un-burnt coal is known as un-burn losses. In pulverized firing system, excessive fines may cause the higher un-burnt loss. In gas fired system, vaporizes light oil contained in the gas can condense, when the gas is expanded in a pressure reducing station. The condensed oil can carbonized in the gas burner and cause poor fuel distribution, which cause incomplete combustion.

E. Pre heat the combustion air:

The waste hot flue gas has enough heat to raise the temperature of combustion air before using for the combustion. Thus waste heat can be recovered from the boiler flue gas. Approximately, 1% thermal efficiency will be increased by raising air temperature by 20°C.

Pre heated combustion air is supplied to the burner, which properly mix this air with fuel and fires into the boiler. Most oil & gas burner in the existing boiler system cannot withstand high air temperature. Which can beraised the combustion efficiency of boiler.

F. Controlling the excess air:

Excess air is the additional air supplied beyond the theoretical air to ensure the complete combustion of fuel, so that C, H, & S of fuel are converted into CO₂, H₂O, & SO₂ respectively. Excess air is supplied to the combustion of fuel because a boiler firing without sufficient air or “fuel-rich” is operating in a potentially dangerous condition. So, excess air is supplied to the burner to provide a safety factor above the actual air required for combustion. A quality design will allow firing at minimum excess air levels of 15% (3% of O₂). O₂ represents oxygen in the flue gas. Excess air is measured by sampling the O₂ in the flue gas. If 15% excess air exits, the oxygen analyzer would measure the O₂ in the excess air & shows a 3% measurement.

The optimum excess air level is depending on burner design & type, furnace design, fuel and process variables. It can be estimated by conducting various performance tests with different fuel/air ratios.

G. Boiler load fluctuation:

The load on the boiler is fluctuating in nature. The efficiency of boiler varies according to load. As load is suddenly increased, steam demand is also increased and pressure will be dropped. Burner is start to fire at its full rate to meet this demand, but pressure continues to drop because boiler is taking some time to respond. Similarly, if load is suddenly decreased, steam demand is reduced and steam pressure is increased, burner immediately lower the firing rate, but again it will take some time, so that steam pressure over shoots the relief valve setting. The maximum efficiency of boiler will occur at nearly 70-85% of full load. Beyond or under this load limits, the efficiency will be decreased

- As the load falls, the fuel & air supply is reducing; hence mass of flue gas will be reduced. The reduction in flow rate of flue gas for some heat transfer area will also reduce the exit flue gas temperature. These all raise the efficiency of boiler.
- As the load falls below 50%, most combustion appliances need more excess air to burn the fuel completely. This increases the sensible heat loss and lowers the boiler efficiency.

Thus, boiler should be operated near to full load for achieving the maximum efficiency.

H. Boiler retrofitting or replacement:

Boiler retrofitting or replacement needs a lot of consideration and should be replaced after detailed energy audit, financial study and feasibility reports. The potential energy saving from replacing a boiler plant depends on the anticipated change in overall efficiency. A change in a boiler plant should be done if existing plant is:

- Old and inefficient
- Over or under sized for present requirements
- Not able to fire cheaper substitute fuel
- Not design for present load conditions.
- Excessive operation & management costs and complexity and not justify.
- Excessive pollution creates from generating unit.

The fuel saving by replacing a boiler of higher efficiency can be estimated as:

$$\text{Fuel saving} = \frac{\eta_{\text{new}} - \eta_{\text{old}}}{\eta_{\text{new}}} * \text{Efficiency consumption}$$

Where,

η_{new} = efficiency of new boiler

η_{old} = efficiency of old boiler

I. Reduce scale and soot formation:

Formation of deposits (scales and soot) on water sides or gas sides can reduce the heat transfer and increase the flue gas temperature. The deposits are like a thermal insulation on the tubes, they must be cleaned periodically for better heat transfer and better efficiency.

Reduction of scaling on water side:

- By proper water treatment and blow down
- Cleaning the tubes at shut down period

These deposits are corrosive and may damage to the water tubes in the boiler furnace, economizer, and air preheater or super heater. Thus deposits can reduce the efficiency of all heat exchangers throughout the flue gas path.

Reduction of soot on gas sides

- Use of soot blowers, soot blowers are used to soot out the deposits from the tube surface and clean the heat transfer surface by utilizing steam at high pressure. Stack temperature should be recorded regularly, when the flue gas temperature increased about 20°C above the normal value, soot blowers are operated and remove the soot deposits. It is advisable to install a dial type thermometer at the stack to monitor the exhaust flue gas temperature.
- Periodic off line cleaning of furnace surfaces, tube banks, heat recovery equipment.

J. Reduce surface heat losses:

Radiation and convection heat losses are the surface heat loss depends on surface temperature and ambient temperature. The boiler surface temperature is higher than surrounding ambient temperature; hence heat is naturally flows from high temperature zone to low temperature zone. Wind velocity also affects these losses.

Surface heat losses are depending on:

- Difference of the temperature between boiler surface and ambient.
- Surface area
- Wind velocity

Surface heat losses are fixed energy losses and do not depend on the boiler loadings. Its value is about 1-5% at full load but contribute about 6% of total losses at 25% load. These losses can be reduced by installing a proper thermal insulation over the outside surface and good refractory lining inside the boiler furnace.

K. Combustion control system improvements:

Conventional combustion control systems are inefficient. Microprocessor based combustion control system is most efficient, reliable and flexible. It has continuous on line sensors that measure and display the gas temperature, oxygen, fuel to air ratio, combustion efficiency etc.

The main components of this system are oxygen sensors, electronic controller and air flow control unit. Oxygen sensors measure the % O₂ and appropriately changes the air flow to the boiler furnace, thus maintain optimum excess air level or optimum fuel/air ratio. Major advantages of this system are that, it is flexible and programmable, operator can change the set points by protective programming of the system.

L. VSD for fans, blowers and pumps:

Variable speed drives are available for variety of applications and equipment for better speed control with reduction in power consumption. The power consumption by fan or pump is directly proportional to cube of speed. Hence little speed reduction can reduce significant power consumption.

Boiler system contains fans, blowers, and pumps for various purposes.

Fans - primary air fan, secondary air fan

Blowers - air blowers

Pump - feed water pump, condensate pump

These all equipment uses an electric motor as a prime mover. VSD can be installed in the existing system to control the speed of electric motor, which is coupled with impeller of fan, blower or pump. There are number of process fans and pumps, a sum of energy saving for each of them by VSD is a big value. Damper control for speed variation is very efficient method.

VIII. CONCLUSION

Conclusion derived from the data related to the boiler, if higher GCV coal is used, then the efficiency should be increased. Ash and Moisture content inside the fuel will affect the efficiency. Here by using semi bituminous coal efficiency is 80.20% because of its high heating value and less moisture and ash content, while Indian lignite coal gives 77.51% efficiency on the same boiler because of it has a more ash and moisture contents than the semi bituminous coal. From this Indirect Method mathematical model, the efficiency should be easily calculated. Simulation should be carried out by the adding different value of data. With the help of simulation, necessary changes should be carried out for the

improving boiler and steam system efficiency. Parameters which can be improved the boiler efficiency is gives a best rest, if they are applies to the boiler system.

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